

CCS WORKSHOP

Jakarta, 22 February 2011

16:00 – 16:25

7. CO₂ Membrane Separation

Teruhiko Kai and Shingo Kazama

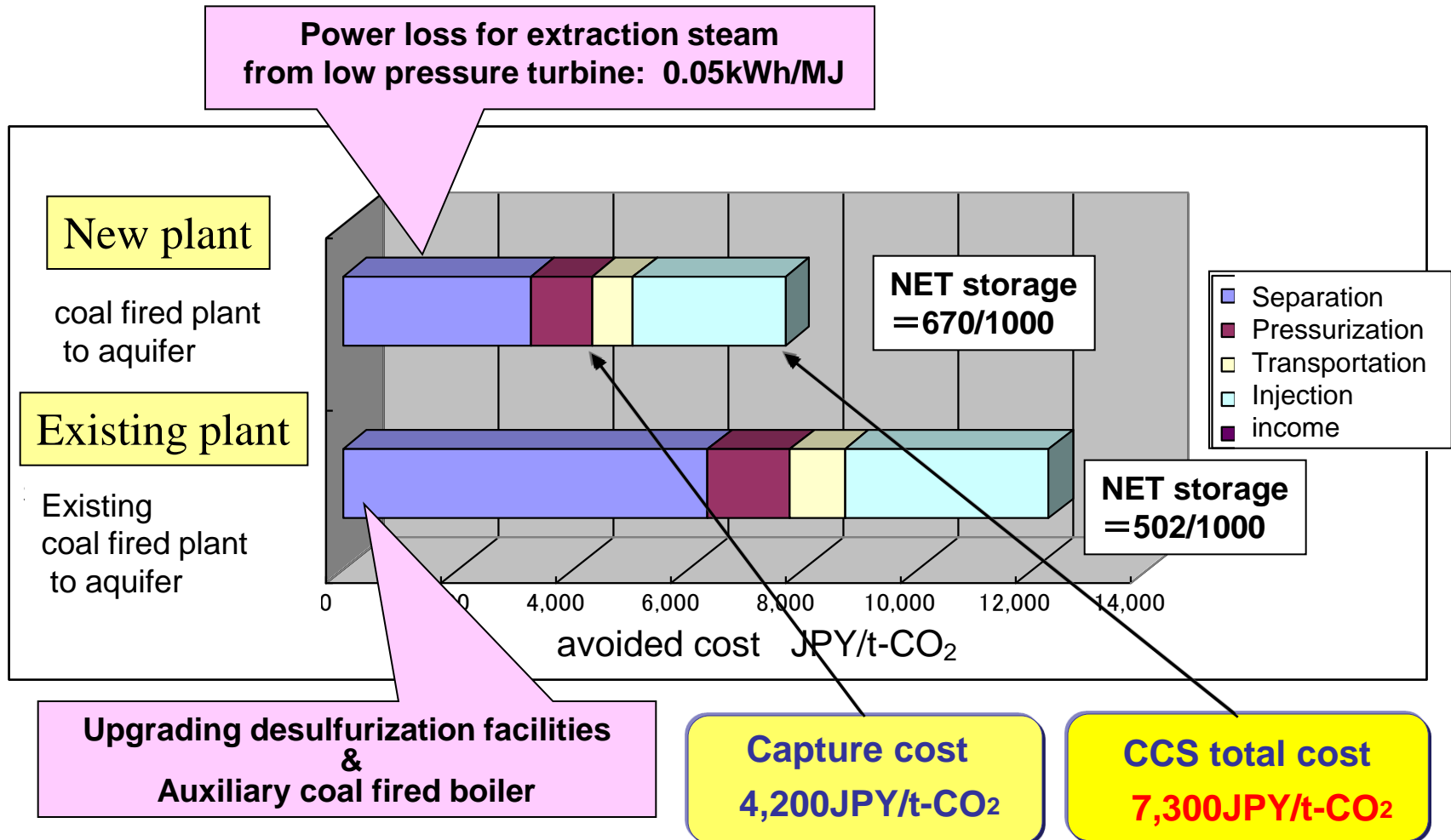
Chemical Research Group

Research Institute of Innovative Technology for the Earth
(RITE)



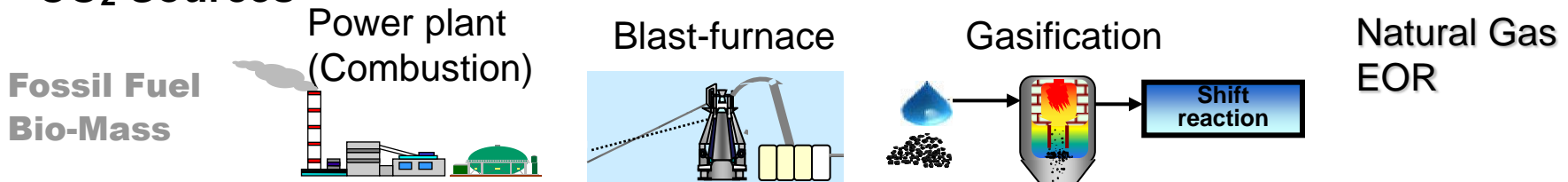
Present Cost of CCS (coal fired power plant)

recovery amount:1Mt-CO₂/yr、 distance:20km、 pressure:7MPa
injection method:ERD、 injection amount :0.1Mt-CO₂/yr/well



CO₂ capture methods for various Sources

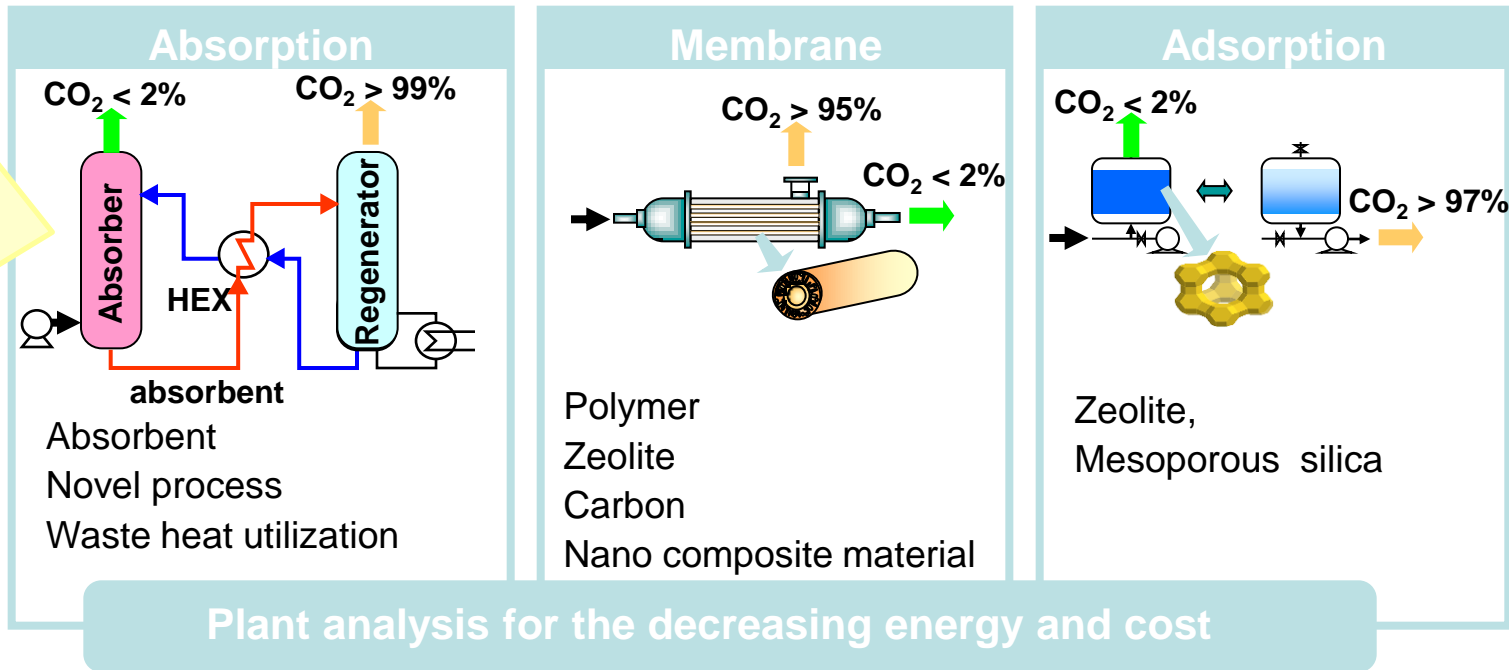
1. CO₂ Sources



2. CO₂ Capture (Chemical Research Group) R. & D.



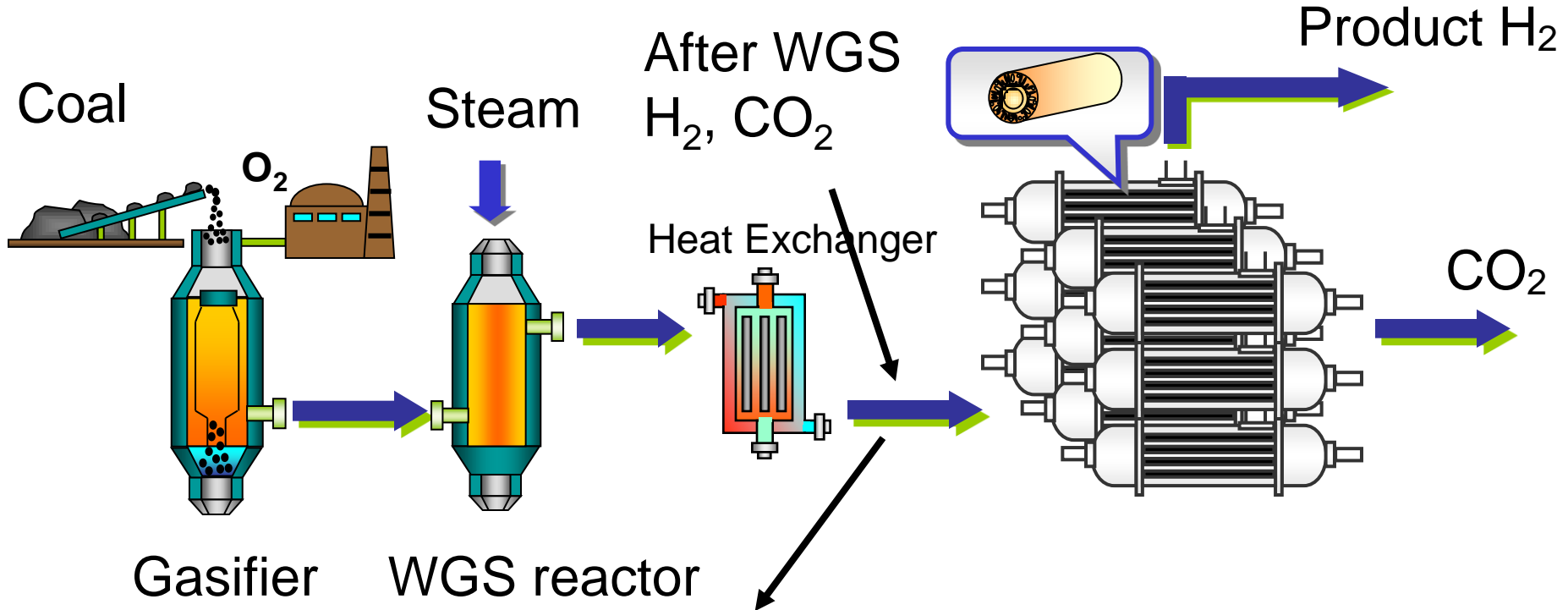
Chemical absorption pilot Plant
(COURSE50: NEDO Project)
Source: Nippon Steel Eng. HP.



3. Storage (CO₂ Storage Group)

Geological Utilization Ocean

Schematic of IGCC with CO₂ Capture



-2 to 4 MPa
-ca 40%CO₂
-CO₂/H₂
Separation

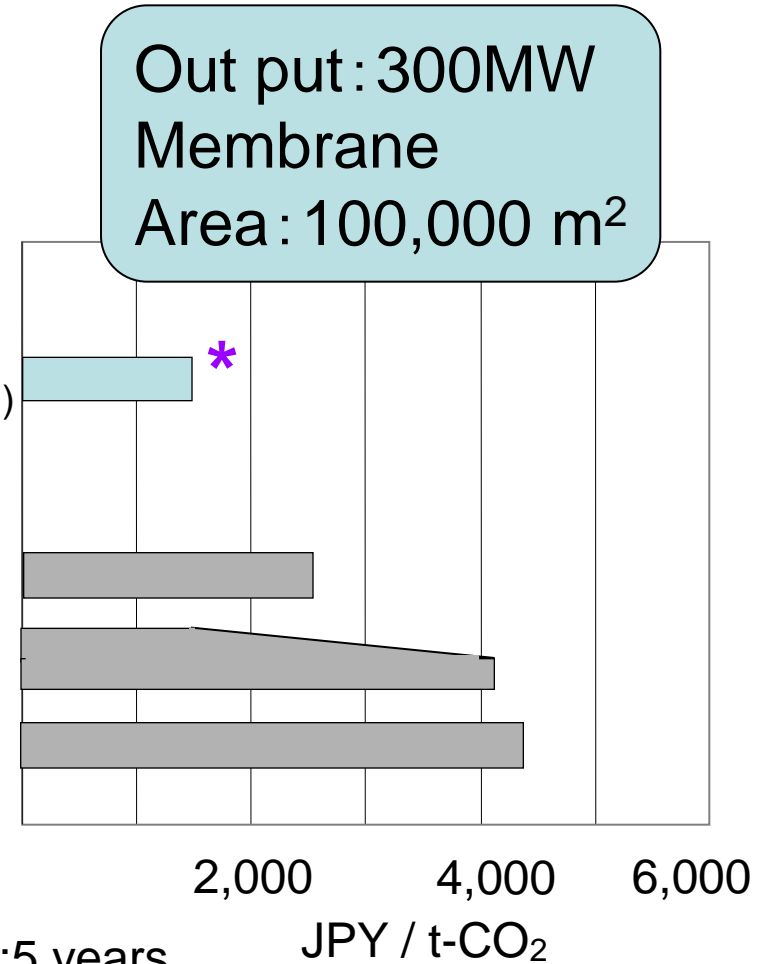
Advantage in
Membrane
Separation
Insufficient
Selectivity

Prospect for CO₂ Separation Cost of Membrane Separation

CO ₂ Source	Gas Pres.	Gas Comp.	Membrane Performance (Target)
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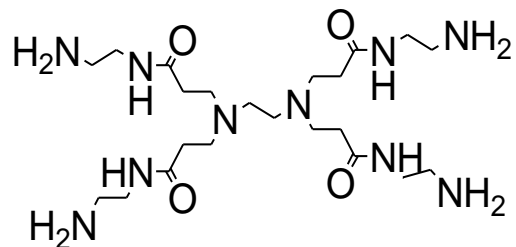
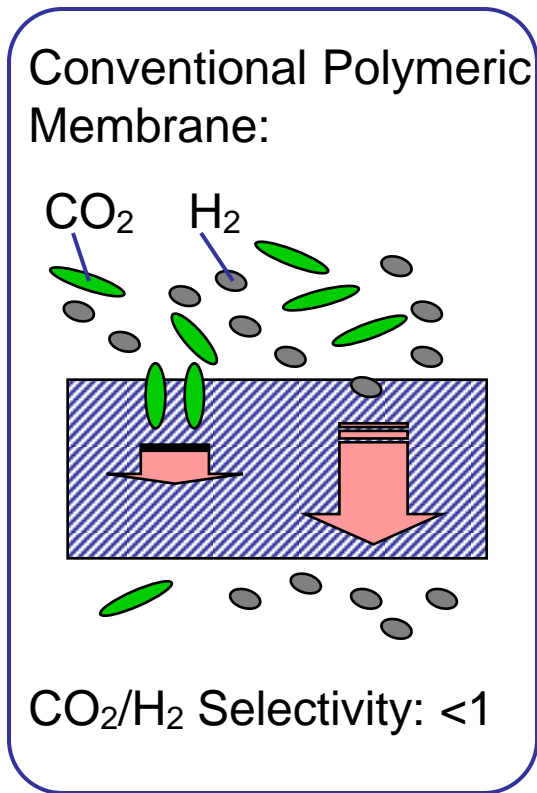
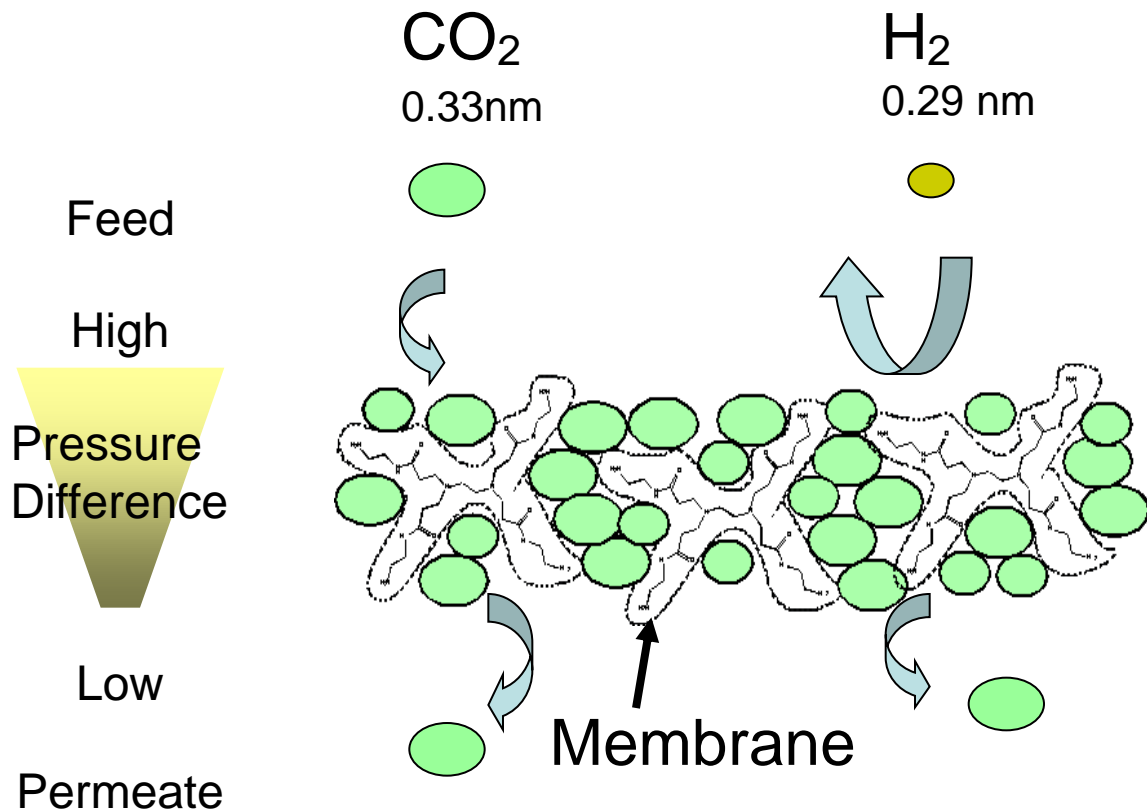
H ₂ Prod. Plant	4MPa	CO ₂ :40% H ₂ , H ₂ O	$\alpha_{CO_2/H_2}: 30$ CO ₂ Permeance : $1 \times 10^{-9} (\text{m}^3 \text{ m}^{-2} \text{ s}^{-1} \text{ Pa}^{-1})$
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Ref. Absorption	4MPa	Amine solution (MDEA-Flash)	
	4MPa	Phys Absorption	
	0.1MPa	Amine solution (KS solution)	



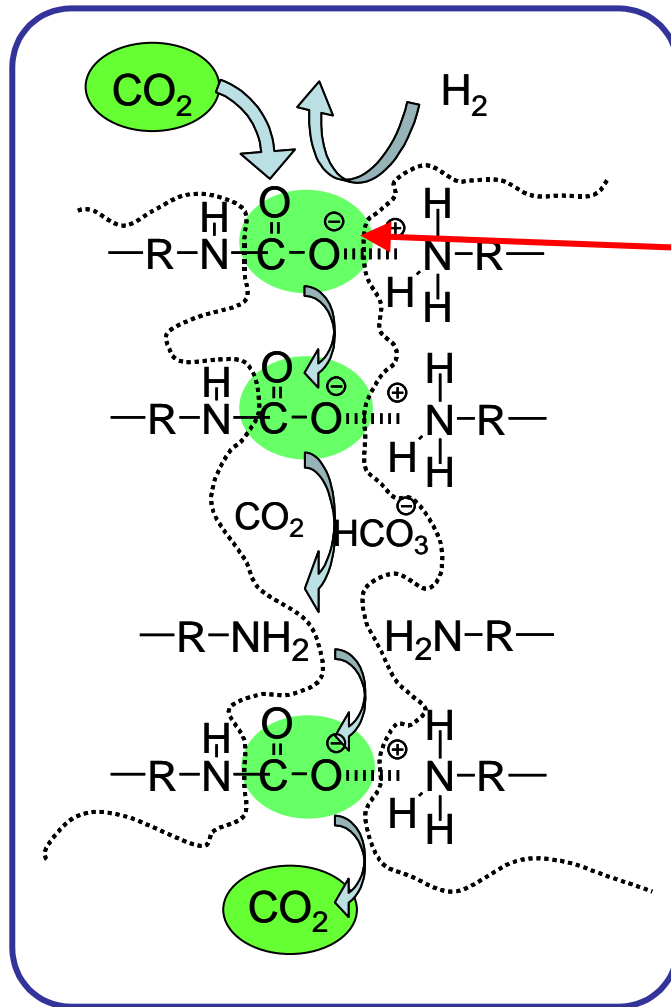
* Duration period Facility:15 years Membrane:5 years
Membrane Skid Cost: 50,000JPY/m²

CO₂ Molecular Gate for CO₂/H₂ Separation

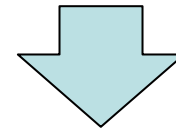


Excellent CO₂ selectivity

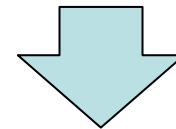
Possible Model of H₂ Perm. Blockage



Carbamate Formation

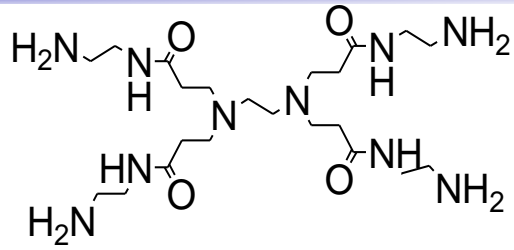
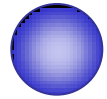


Pseudo-cross-linkage

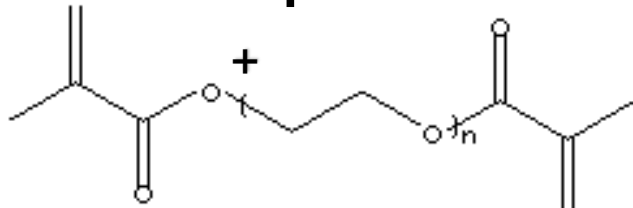


H₂ permeation blockage

Dendrimer Membrane for CO₂ Capture from Pressurized Gas Stream

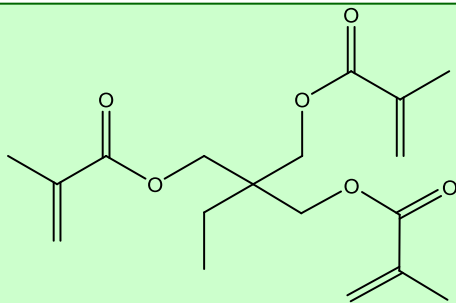


O-OH-PAMAM dendrimer



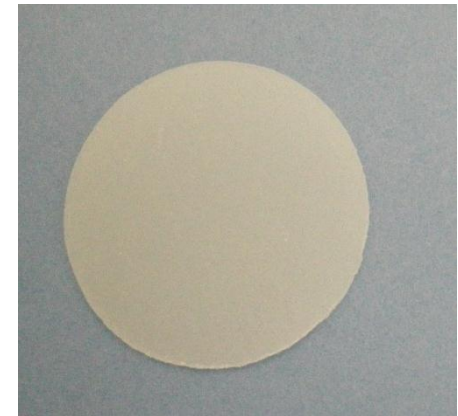
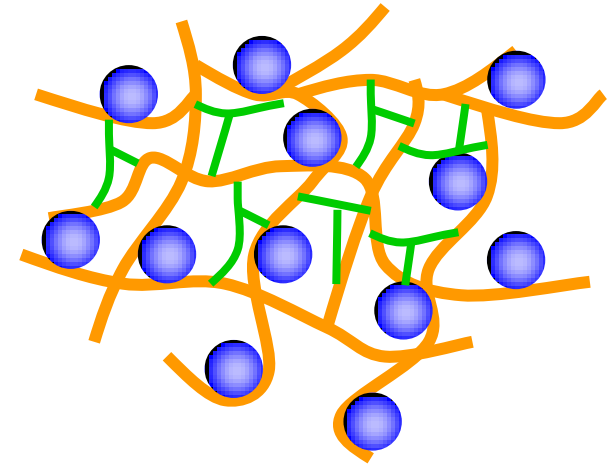
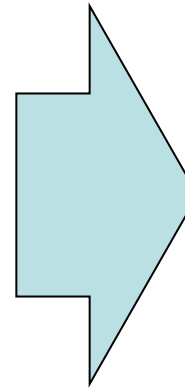
PEGDMA

+

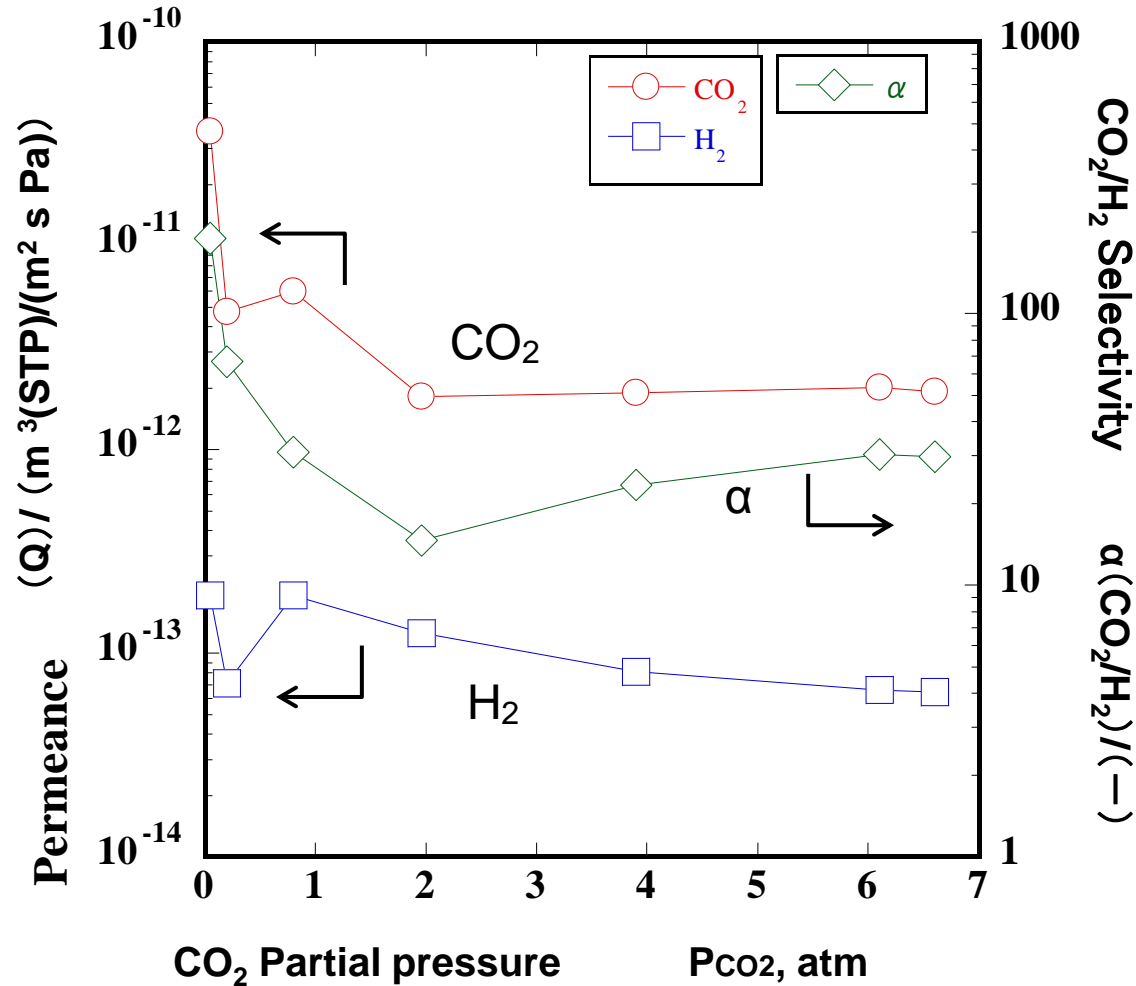


TMPTMA

UV
Curing

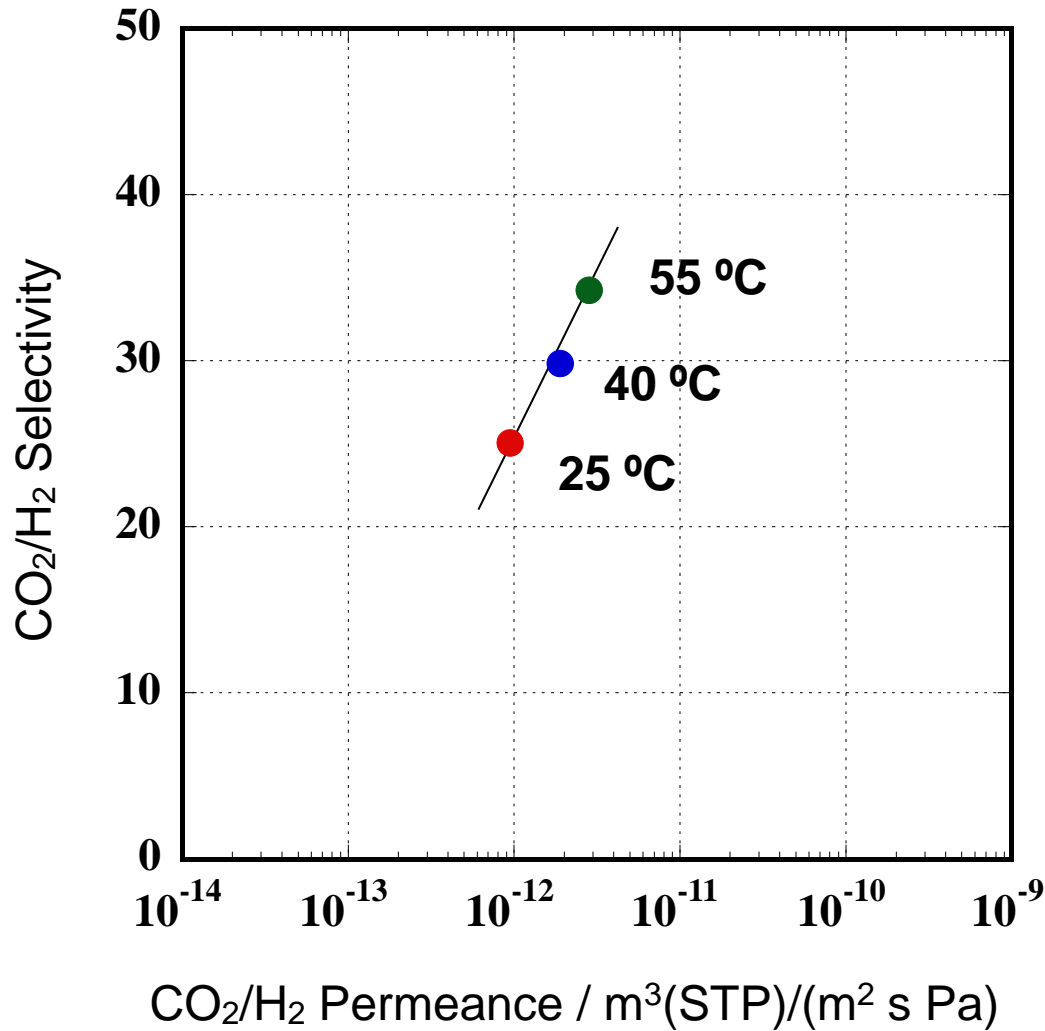


Dendrimer membrane for CO₂ capture from a pressurized gas stream



PAMAM/PEGDMA/TMPTMA = 50/37.5/12.5, Feed : 100 mL/min, Sweep : 20 ml/min, T = 313 K, R.H. = 80%

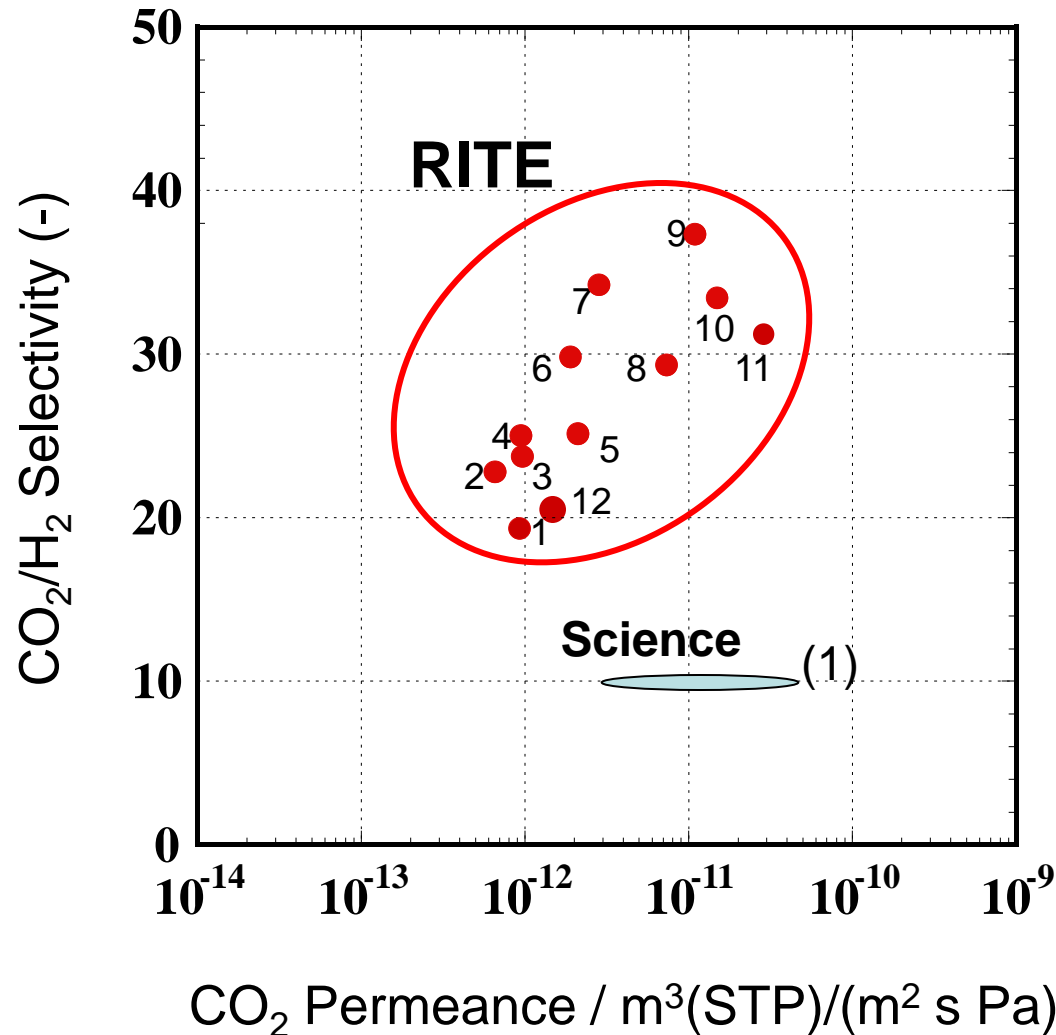
Temperature and Performance



PAMAM/
PEGDMA/
TMPTMA =
50/37.5/12.5

Thickness: 500μm

CO₂/H₂ Separation Properties of Dendrimer Membranes at High Pressure



(1) H. Lin, B. Freeman *et al.*, *Science*, **311**, 639-642 (2006)

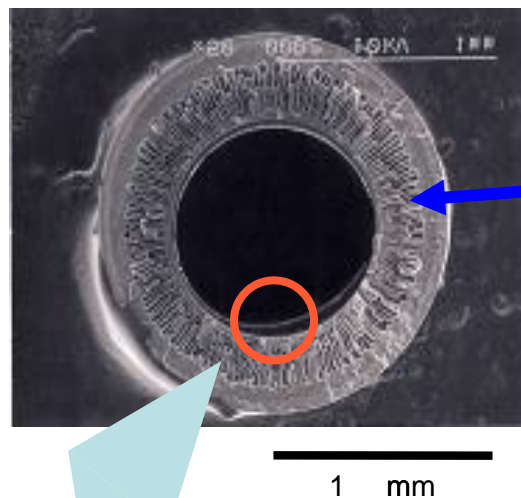
Separation of CO₂/CH₄ using molecular gate membranes

	CO ₂ conc. in Feed	CO ₂ conc. in Permeate	Permeance, Q _{CO2}	Separation factor, $\alpha_{\text{CO}_2/\text{CH}_4}$
Membrane A	79.6	99.2	7.6×10^{-12}	30
Membrane B	74.5	99.9	1.2×10^{-11}	260

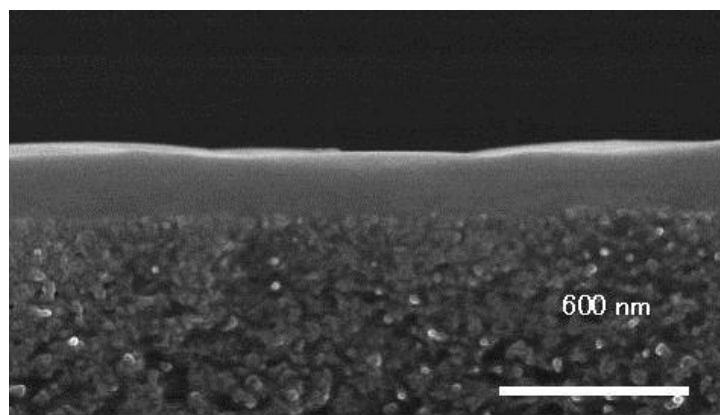
Temperature: 40 °C, Total pressure in feed gas: 0.1 MPa,
Relative humidity in Feed gas: 80%, He sweep gas at permeate side.

**Molecular gate membranes possess high potential
for separation of CO₂/CH₄ mixed gas**

Dendrimer Composite Membrane



Substrate of
UF Membrane
(commercial)

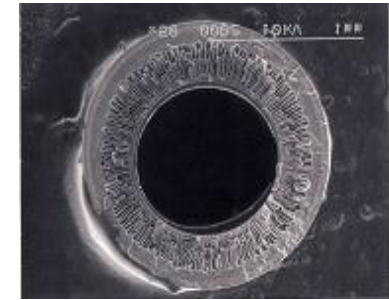


Selective Layer
OOH Dendrimer/
Polymeric Matrix

Porous Substrate

For CO₂ separation from ambient pressure gas stream (1st Term)

Dendrimer Composite Membrane Module



1 mm

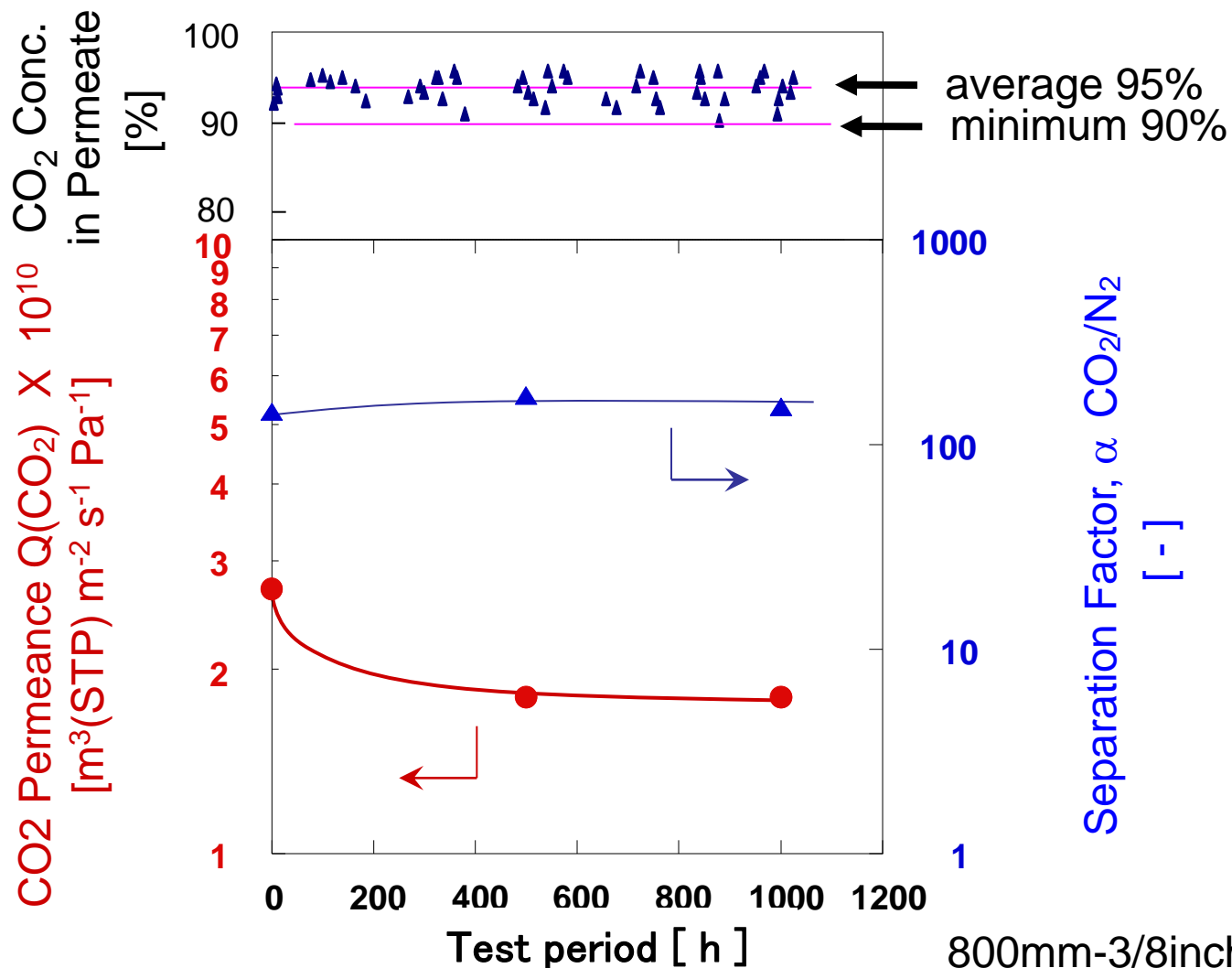
Cross section of membrane

Module #	Membrane Area cm ²	CO ₂ /N ₂ Selectivity $\alpha_{\text{CO}_2/\text{N}_2}$
1	17	290
2	180	150
3	4000	150

Dendrimer: conventional PAMAM dendrimer (0OH), Temperature: 25 °C

For CO₂ separation from ambient pressure gas stream (1st Term)

Long-term Stability



800mm-3/8inch module

Feed gas mixture: CO₂/N₂ (32/68 v/v%) containing unknown amount of water vapor
 Measured temperature: 14-25°C, Pressure difference between feed and permeate: 0.1MPa

Membrane modules

Hollow-fiber module:

Merits:

- Well-studied structure for gas separation
- Large membrane area per unit volume

Issues:

- Pressure durability up to 4MPa
- Coating method for hollow-fibers

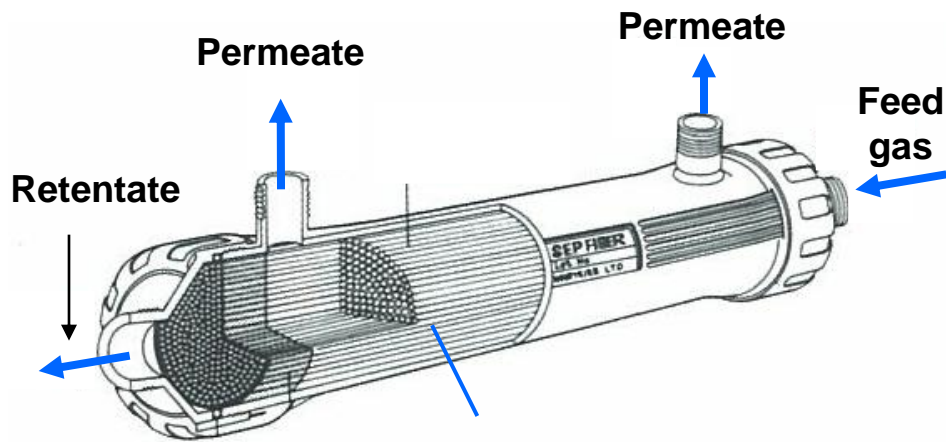
Spiral-wound Module (flat-sheet membranes):

Merits:

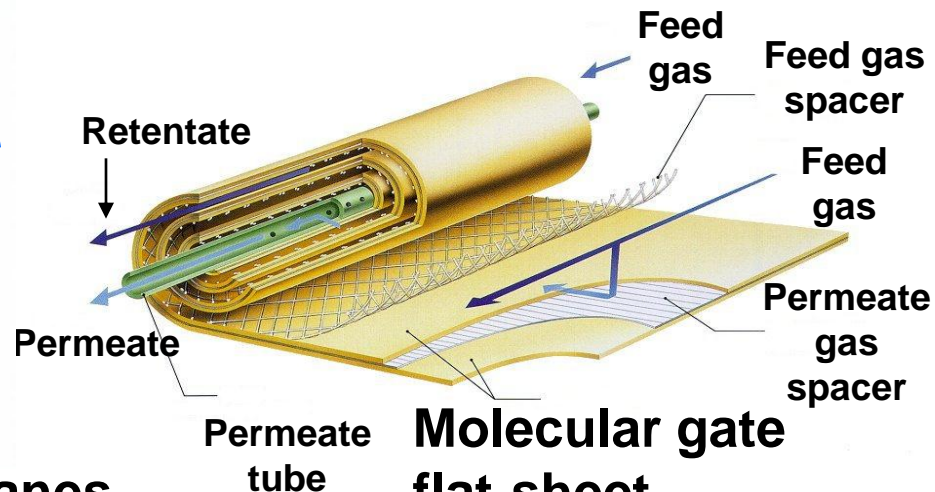
- Pressure durability up to 10MPa (water)
- Easy to coat flat-sheet membranes

Issue:

- Membrane area per unit volume



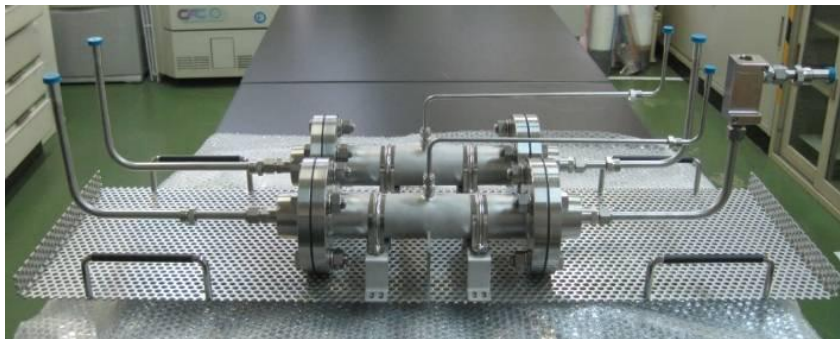
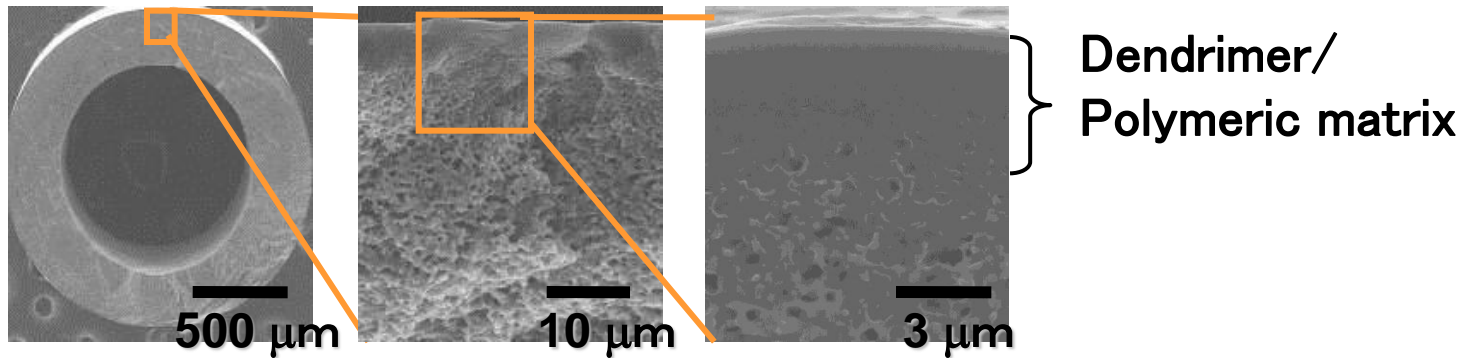
**Molecular gate
Hollow-fiber membranes**



**Molecular gate
flat-sheet
membranes**

Cooperation with private companies (Development of Membrane module)

Cooperation with
Four membrane companies (Kuraray, Daicel, Toray, Nitto-Denko)
Engineering company (Nippon Steel Engineering)



Membrane module test using syngas



Testing apparatus at ECOPRO Gasifier, Nippon Steel Corporation (Yawata plant), Nippon Steel Engineering Co., Ltd.

Acknowledgements

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- Ministry of Economy, Trade and Industry (METI), Japan.
- Nippon Steel Engineering Co., Ltd.



*Thank you for
your attention!*

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